Study on Operating Characteristics of Power Plant with Dry and Wet Cooling Systems

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ABSTRACT

The present paper will study the performance of the power plant with the combination of dry and wet cooling systems in different operating conditions. A thermodynamic performance analysis of the steam cycle system was performed by means of a program code dedicated to power plant modeling in design operating condition. Then the off-design behavior was studied by varying not only the ambient temperature and relative humidity but also several parameters connected to the cooling performance, like the exhaust steam flow rate, the air cooling fan load and the number of operating cooling water pumps and cooling towers. The result is an optimum set of variables allowing the dry and wet cooling system be regulated in such a way that the maximum power is achieved and low water consumption.

Keywords: Dry and Wet Condenser; Cooling Tower; Off-design; Characteristic Curve; Operational Optimization

1. Introduction

There are three ways of thermal power plants’ cooling systems: dry cooling system, wet cooling system, and dry and wet cooling system. In China, the wet cooling system use in the power plants commonly, but in the northwest and northeast China where the water is shortage use air cooling system. The wet cooling systems have high thermal economy, but with high water consumption. The air cooling systems can save a lot of water, but the exhaust steam pressure is high and varying all the time for the impact of ambient temperature [1]. The wet and dry cooling systems combines the both advantages, it not only make full power when the ambient temperature is high but also with low water consumption [2,3].

The present study was inspired by the operation of a power plant with the combined wet and dry cooling system (Figure 1), placed in Northwest China. The wet and dry cooling system is composed of an air cooled condenser in parallel with a water cooled condenser. In the wet cooling system, the cooling water which shared by two 300 MW Units, taken from the condenser passes through four wet mechanical draft cooling towers and returns to the condenser by two cooling water pumps.

The off-design performance of an air cooling condenser or water cooling condenser separately is well deeply investigated [4-6], but the study on the performance of complies wet and dry cooling system is rarely find. So the critical element of this study is the wet mechanical draft tower. The heat transfer in cooling tower is a very complex phenomenon. But it could be described by several equations [7-9] with some simplifying assumptions.

The purpose of the present paper is to explore the impact of a dry and wet cooling system on the thermo-dynamic performance of a power plant. This paper offers an original contribution for cooling system performance analysis by considering the dry and wet system together.

2. Mathematical Model of Direct Air Cooling System

2.1. The Pressure of Air Condenser

Using η-NTU method to calculate the condensate temperature of air condenser [1]:

\[ t_{sat} = \frac{D_c (h_x - h_{sat})}{S_{sat} Y_{sat} \rho_c C_p} \frac{1}{1 - e^{-\eta NTU}} + t_{sat} \]  \hspace{1cm} (1)

Figure 1. Schematic of the wet and dry cooling systems.
\[
NTU = \frac{KS}{100S_y v_y P_a \rho_c^2} \quad (2)
\]

where: \( D_c \) is exhaust steam flow rate. \( h_c \) is condensate enthalpy. \( h_c' \) is exhaust steam enthalpy. \( t_{as} \) is ambient temperature. \( S_y \) is frontal area. \( v_y \) is face velocity. \( \rho_a \) is air density. \( NTU \) is heat transfer units. \( K \) is heat transfer coefficient. \( S \) is total area.

Using Equation (3) to calculate the condenser pressure of air condenser:
\[
p_{s1} = 9.81 \times \left( \frac{t_{s1} + 100}{57.66} \right)^{0.46} \quad (3)
\]

Exhaust steam pressure is:
\[
p_c = p_{s1} + \Delta p_1 \quad (4)
\]

where: \( \Delta p_1 \) is air condenser pressure drop.

### 2.2. Air Cooling Condenser Heat transfer Coefficient

The total heat transfer resistance including internal thermal resistance, external thermal resistance, and wall thermal resistance:
\[
\frac{1}{KS} = \left( \frac{1}{\alpha_i} + \varepsilon_i \right) + \frac{1}{S_y} \lambda_b S_m + \left( \frac{1}{\alpha_o} + \varepsilon_o \right) \frac{1}{\eta_0 S_{out}} \quad (5)
\]
\[
S_m = (S_0 - S_i) / \ln(S_0 / S_i) \quad (6)
\]
\[
\eta_0 = (S_0 + \eta_f S_{fin}) / S_{out} \quad (7)
\]

where: \( K \) is total heat transfer coefficient. \( S \) is total area. \( \alpha_i \) and \( \alpha_o \) are internal and external tube convective heat transfer coefficient. \( \varepsilon_i \) and \( \varepsilon_o \) are internal and external tube fouling resistance. \( \delta_b \) is base pipe wall thickness. \( \lambda_b \) is base pipe wall thermal conductivity. \( S_i \) and \( S_0 \) are internal and external surface area of tubes. \( S_m \) is the number heat transfer area of the base pipe. \( S_{fin} \) is fin surface area. \( S_{out} \) is outer heat transfer area. \( \eta_f \) is fin efficiency. \( \eta_0 \) is the total tube fin efficiency.

### 3. Mathematical Model of Water Cooling System

#### 3.1. The Pressure of Water Condenser

Water condenser temperature could be got by Equation (8):
\[
t_{s2} = t_{wi} + \frac{h_c - h_c'}{4.187 \left[ 1 + \frac{1}{4.187 m} \right]} \quad (8)
\]

where \( m = D_o / D_c \) is circulation ratio. \( D_o \) is steam flow rate. \( D_c \) is cooling water flow rate. \( h_c - h_c' \) is 1kg steam’s latent heat. \( t_{wi} \) is cooling water temperature to condenser. \( K \) is heat transfer coefficient. \( A \) is cooling area.

Then the water condenser pressure \( p_{s2} \) can be calculated by Equation (3), the exhaust steam pressure is:
\[
p_c = p_{s2} + \Delta p_2 \quad (9)
\]

where: \( \Delta p_2 \) is water condenser pressure drop.

#### 3.2. Cooling Water Temperature to Water Condenser

In a closed-loop cooling water system, cooling water temperature to condenser equals cooling water temperature from cooling tower, it is not only affected by environmental conditions, but also by the design parameters and operating conditions of the cooling tower.

At present, the cooling tower thermodynamic calculation use enthalpy method commonly [7,8]. The equations are not shown in this paper.

### 4. Results and Discussion

The power plant with dry and wet cooling systems can operate as three cases: direct air cooling (Dry), dry and wet cooling system with one cooling water pump and two wet mechanical draft towers (D&W_1), and dry and wet cooling system with two cooling water pumps and four wet mechanical draft towers (D&W_2). Assuming two Units at the same operating conditions, each Unit can get half of the circulating cooling water flow rate.

In order to optimize the operation, it must study the respective operating conditions off-design characteristics fistly.

#### 4.1. Design Parameters

Table 1 shows the main design parameters of the Unit with wet and dry cooling systems.

Each considered variable is subjected to the constraints listed in Table 2, it contains any possible the power plant operating condition during the year.

<table>
<thead>
<tr>
<th>Name</th>
<th>Unit</th>
<th>Content</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ambient temperature</td>
<td>°C</td>
<td>23.6</td>
</tr>
<tr>
<td>Atmospheric pressure</td>
<td>kPa</td>
<td>90.06</td>
</tr>
<tr>
<td>Relative humidity</td>
<td>%</td>
<td>86.84</td>
</tr>
<tr>
<td>Gross power output</td>
<td>MW</td>
<td>300</td>
</tr>
<tr>
<td>Exhaust steam flow rate</td>
<td>t/h</td>
<td>614.23</td>
</tr>
<tr>
<td>Exhaust steam enthalpy</td>
<td>KJ/kg</td>
<td>2437.9</td>
</tr>
<tr>
<td>Exhaust steam pressure</td>
<td>kPa</td>
<td>15</td>
</tr>
<tr>
<td>AC cooling area</td>
<td>m²</td>
<td>492 810</td>
</tr>
<tr>
<td>AC frontal area</td>
<td>m²</td>
<td>5128</td>
</tr>
<tr>
<td>AC face velocity</td>
<td>m/s</td>
<td>2.91</td>
</tr>
<tr>
<td>Wet condenser cooling area</td>
<td>m²</td>
<td>3700</td>
</tr>
<tr>
<td>Cooling water flow rate</td>
<td>t/h</td>
<td>12100</td>
</tr>
<tr>
<td>Gas-water ratio</td>
<td>/</td>
<td>0.506</td>
</tr>
<tr>
<td>CT cooling number</td>
<td>/</td>
<td>1.12</td>
</tr>
</tbody>
</table>
4.2. Dry configuration

The exhaust steam flow rate and ambient temperature influence on exhaust pressure can be got by using mathematical model of direct air cooling systems mentioned before. Figures 2-5 reports some of the parametric analysis results for the Dry configuration. As can be seen from these Figs, the exhaust pressure rise with exhaust steam flow rate increases and ambient temperature rises. And the higher the ambient temperature, this trend is more obvious. The exhaust pressure will drop when AC fan load increases. The AC fan load should be operated according to the maximum load to get the highest power production, because auxiliary power consumption will rise as AC fan load rising.

<table>
<thead>
<tr>
<th>Input variables</th>
<th>Unit</th>
<th>Ranges</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ambient temperature</td>
<td>°C</td>
<td>-20 - 35</td>
</tr>
<tr>
<td>Relative humidity</td>
<td>%</td>
<td>20 - 100</td>
</tr>
<tr>
<td>Air condenser fan load</td>
<td>%</td>
<td>10 - 100</td>
</tr>
<tr>
<td>Exhaust steam flow rate</td>
<td>t/h</td>
<td>250 - 650</td>
</tr>
</tbody>
</table>

4.3. W & D Configuration

The wet and dry cooling system off-design process was carried out by excel VBA code by using the mathematical model mentioned before. Table 3 compares the model results against experimental date in three cases. The three cases show three different environmental conditions and power output. For all the cases, a good agreement was found between model results and experimental date: the maximum difference is lower than 5%.

Figures 5-10 show the influence of the parameters mentioned before on exhaust pressure and dry proportion from W&D model.

Figure 4 shows the exhaust pressure variation versus ambient temperature and relative humidity. As expected, exhaust pressure increases with rising relative humidity. The effect becomes more and more appreciable with increasing temperature. In the same range of ambient temperature changes, the greater the relative humidity the more obvious exhaust pressure changes. This is consistent with the dry proportion behabious shown in Figure 6.
it is obvious that the steam flow rate entering the AC increases with raise in relative humidity. Relative humidity increases, the heat transfer capacity of the cooling tower decline, so wet proportion decreases.

The influence of the AC fan load on the cycle performance is shown in Figures 7-8. Obviously, the exhaust pressure decreases with rising AC fan load. The effect becomes more and more appreciable with increasing temperature. The steam flow rate entering the AC increases with raise in AC fan load.

Table 3. Comparison between model result (M) and experimental data (EXP).

<table>
<thead>
<tr>
<th>Case 1</th>
<th>Case 2</th>
<th>Case 3</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Ambient temperature(℃)</td>
<td>22</td>
<td>30</td>
</tr>
<tr>
<td>Relative humidity (%)</td>
<td>68</td>
<td>48.3</td>
</tr>
<tr>
<td>Power output (MW)</td>
<td>300</td>
<td>265</td>
</tr>
<tr>
<td>Exhaust steam flow rate (t/h)</td>
<td>614.23</td>
<td>540</td>
</tr>
<tr>
<td>Steam flow rate to wet (t/h)</td>
<td>273.216</td>
<td>255.11</td>
</tr>
<tr>
<td>Air condenser fan load (%)</td>
<td>93</td>
<td>93</td>
</tr>
<tr>
<td>Cooling water temperature from CT(℃)</td>
<td>29.287</td>
<td>34.3</td>
</tr>
<tr>
<td>Cooling water temperature to CT (℃)</td>
<td>38.394</td>
<td>42.804</td>
</tr>
<tr>
<td>Exhaust steam Pressure KPa</td>
<td>14.707</td>
<td>13.64%</td>
</tr>
</tbody>
</table>

Figure 6. Relative humidity and ambient temperature influence on dry proportion - W&D.

Figure 7. AC fan load and ambient temperature influence on exhaust pressure - W&D.

Figure 8. AC fan load and ambient temperature influence on dry proportion - W&D.

Figure 9. Exhaust steam flow rate and ambient temperature influence on exhaust pressure - W&D.
The influence of the exhaust steam flow rate on the cycle performance is shown in Figures 9-10. The exhaust pressure progressively increases with exhaust steam flow rate increases. The effect becomes more and more appreciable with increasing temperature. The way in which the exhaust steam is shared into the two condensers is shown in Figure 10, that a decreasing steam flow rate goes through the air cooling system as the ambient temperature increases from 10°C to 25°C, but an increasing team flow rate goes through the air cooling system as the ambient temperature increases from 30°C to 35°C. This behaviour is consistent with the water cooling condenser has better performances in high temperature.

4.4. Optimization of the Operation

At the low temperature, the unit operate with direct air cooling system. Figure 11 report the results of the condensing system optimization procedure for the Dry configuration. The AC fan load which meet the power load at different ambient temperature is given in Figure 11. The AC fan load increases with rising ambient temperature. When the power load is 300MW, it must open D&W₁ at 16°C, and D&W₁ open at 24°C when power load is 225 MW, and D&W₁ open at 31°C when power load is 150 MW. When power load is lower than 120 MW, it’s no need to open D&W₁.

![Figure 10. Exhaust steam flow rate and ambient temperature influence on dry proportion -W&D.](image1)

![Figure 11. Power load and ambient temperature influence on AC fan load – Dry.](image2)

Figures 12-13 report the results of the condensing system optimization procedure for the D&W₁ configuration. The AC fan load which meet the power load at different ambient temperature is given in Figure 12. The AC fan load increases with rising ambient temperature. When the power load is 300 MW, it must open D&W₂ at 24°C, and D&W₂ open at 31°C when power load is 225 MW. When power load is lower than 150MW, it’s no need to open D&W₂.

![Figure 12. Power load and ambient temperature influence on AC fan load – D&W₁.](image3)

Figure 13. Power load and ambient temperature influence on dry proportion – D&W₁.  

Figures 14-15 report the results of the condensing system optimization procedure for the D&W₂ configuration. The AC fan load which meets the power load at different ambient temperature is given in Figure 14. The AC fan load increases with rising ambient temperature. When the power load is 225 MW, the exhaust pressure can keep 15 KPa at any ambient temperature. But when the power load is 300 MW, the exhaust pressure can not keep 15 KPa at ambient temperature is above 28°C.

5. Conclusions

A detailed simulation of a wet and dry cooling system installed in a steam power plant was developed and some conclusions were made as follows:
A parametric analysis was carried out in order to check the influence of ambient temperature, relative humidity, exhaust steam flow rate and air condenser fan load on the thermodynamic performances of a power plant with dry and cooling system.

2) In dry and wet cooling system, the exhaust pressure decreases with rising AC fan load, and increases with rising relative humidity and exhaust steam flow rate. The effect becomes more and more appreciable with increasing ambient temperature.

3) The heat load distribution of dry and wet cooling system in different operation situations was well developed. Steam flow rate to AC decreases with increasing ambient temperature, and increases with increasing air cooling condenser fan load and relative humidity, but when the exhaust steam flow rate increases, steam flow rate to AC may increase or may be decrease decided by the ambient temperature conditions.

4) The air cooled condenser resulted the best way to reject heat if the temperature is lower than 16℃, 24℃, 31℃, when the power load is 300 MW, 225 MW, 150 MW. At higher ambient temperature, the condensation should exploit the cooling capacity of the tower as much as possible while discarding the remaining heat in the air condenser.

REFERENCES


